

Dynamic Plant Simulator for HVAC Systems

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Abstract

The detailed dynamic simulation of coupled units in HVAC-systems and buildings is gaining increasing importance as strong tool in HVAC-engineering and operation. This investigation deals with the basics in the development of an universally applicable dynamic simulator. General fundamentals are formulated some moduls are outlined. Shnulation of a heated 4-room-residence, a solar system and a storage tank as applications demonstrate the mode of functioning and the potential of the simulator.

1. Introduction

In order to analyse energy consumption of HVAC systems in buildings, the dynamic behaviour in the time dornaine of thermal components and HVAC equipment, operating in buildings has to be investigated. Thermal characteristics of all cornpoilents, including the building have to be related to the physical conditions Imposed by the surroundings. As usefull in large systems a universally applicable dynamic simulation model has been conceived and for application to HVAC systeins in buildings developed.

In this modular approach the complete system is considered to be a collection of integrated subsystems, each as niodule having identifiable physical characteristics and beeing modelled as precisely as desirable.

Translating physical equipment and systems to a mathematical form, that can be attached by the mathematics of control systems, results in a mathematical description of dynamic simulation which is that of one single equation of state for the total systein, a matrix-equation as function of state and disturbance, implicitly to be solved, [11, [21.

Compared with the explicit Euler-algoritlim of first order the here presented implicit state-space representation is superior with regard to programm ng, processingspeed, accuracy and stability of numerical solution.

The components of an HVAC system, energy-generation or ~transformation, storage and -distribution, interrelated with the random conditions ,weather" and ,eienergy~sotirces" and the building operation, may be modelled independently from each other as subroutine moduls.

This simulation system applies universally as every component of the HVAC sy.stein or of the building can be modelled in analogous way. The dynamic plant simulator is an important tool in HVAC engineering and operation., efficiency analysis, comparison, optimization and optimal design, studies on energy consS111111)tiOn, emission, Costs and new technologies of different HVAC systems may be performed.

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Translating physical equipment and systems to a mathematical form, that can be attached by the mathematics of control systems, results in a mathematical description of dynamic simulation which is that of one single equation of state for the total system, a matrix-equation as function of state and disturbance, implicitly to be solved, [1], [2].

Compared with the explicit Euler-algorithm of first order the here presented implicit state-space representation is superior with regard to programming, processing-speed, accuracy and stability of numerical solution.

The components of an HVAC system, energy-generation or -transformation, -storage and -distribution, interrelated with the random conditions „weather“ and „energy-sources“ and the building operation, may be modelled independently from each other as subroutine moduls.

This simulation system applies universally as every component of the HVAC system or of the building can be modelled in analogous way. The dynamic plant simulator is an important tool in HVAC engineering and operation; efficiency analysis, comparison, optimization and optimal design, studies on energy consumption, emission, costs and new technologies of different HVAC systems may be performed.

2. Dynamic Simulation

2.1 Model and Method

A dynamic HVAC simulation model for thermal processes is consisting of four Components:

climatological data or model, a physical model of the HVAC, system(s), a physical model of the building and a physical model of the operation.

Climatological data, are given by the TRY-data, which are provided by the national weather services in kind of data files.

First step of model development is the translation of the physical equipment and its processes in the time domain by help of the equations of energy balance. As usual in automatic-control the functional relationships and interactions of the component models have been established and represented by the block diagram of the total system - building plus HVAC - in fig. 1.

The blocks represent transfer functions of the components, for example the boiler, the collector of a solar system, the storage tank and the walls of the building. The lines represent the energy flows resp. information-flows between the components. The proceeding when simulating thermal systems at transient state must take into account the time function of the loads, the transient energy flows in the walls and the dynamic energy exchange between the components of the system and e.g. a room as 1 illustrated in fig. 2. The application of the principles of dynamics to the physical components had to be translated into the model.

2.2 Mathematical Formulation and Solution of the System Equations

The described method results in a system of differential equations which has to be solved numerically. In contradiction to a typical modular approach and serial solving of the differential equations, a state matrix formulation was introduced. The principle of the procedure will be demonstrated as follows:

The energy balances of the mass inside a room (air, furniture; index 1) may be

written in the form

written

$\frac{d}{dt}$

$$W_{wall} + Q_{i,F} + Q_{i,V} + Q_{i,H} + Q_{i,t} + Q_L = dt$$

The time derivative of the indoor temperature T_i , the state variable, can then be expressed as a function (state) of the state variables (other temperatures) and the disturbance variables, the outdoor temperature T_o , and the internal energies (for example the heat produced by persons; $Q_{i,t}$); additional introduction of the equation, for heat flow gives

$$\frac{d}{dt} T_i = \frac{1}{W_{wall}} (Q_{i,F} + Q_{i,V} + Q_{i,H} + Q_{i,t} + Q_L - Q_{i,t})$$

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The energy balances of the mass inside a room (air, furniture; index I) may be written in the form

$$m_I \cdot c_I \cdot \frac{d\vartheta_I}{dt} = \dot{Q}_{I,AW} + \dot{Q}_{I,F} + \dot{Q}_{I,IW} + \dot{Q}_{I,H} + \dot{Q}_{int} + \dot{Q}_L \quad (1)$$

The time derivative of the indoor temperature ϑ_I , the state variable, can then be expressed as a function (sum) of the state variables (other temperatures) and the disturbance variables, the outdoor temperature ϑ_A , and the internal energies (for example the heat produced by persons; \dot{Q}_{int}); additional introduction of the equations for heat flow gives

$$\frac{d\vartheta_I}{dt} = a_{I,I} \cdot \vartheta_I + a_{I,AW} \cdot \vartheta_{AWo} + a_{I,IW} \cdot \vartheta_{IWo} + a_{I,H} \cdot \vartheta_H + b_{I,A} \cdot \vartheta_A + b_{I,int} \cdot \dot{Q}_{int}$$

,dj

$$(a_{j,j} \frac{dO_j}{dt} + \sum_{i=1}^n a_{i,j} O_i) = \sum_{i=1}^n b_{i,j} s_i + Q_{int} \quad (2)$$

This equation can be translated into a vector equation (matrix representation)

$$\frac{dO}{dt} = A_{j,j} \cdot O_j + B_{i,j} \cdot s_j \quad (3)$$

with

$A_{j,j}$ matrix of state variables
 O_j vector of state variables

matrix of disturbance

s_i vector of disturbance variables

The coefficients $a_{i,j}$ and $b_{i,j}$ of the influence coefficients of matrix $A_{j,j}$ and $B_{i,j}$ result from the heat transfer coefficient and heat capacities, for example

$$a_{i,j} = -\frac{h_{i,j} A_{i,j}}{C_j} \quad (4)$$

$$b_{i,j} = \frac{h_{i,j} A_{i,j}}{C_j}$$

The partial differential equation of the transient heat transfer in the walls (Fourier's law) is

$$\frac{d^2 T}{dx^2} = \frac{1}{\alpha} \frac{dT}{dt} \quad (5)$$

$$\frac{dT}{dt} = \alpha \frac{d^2 T}{dx^2}$$

Discrete representation of the local differential coefficient of the temperature, assumed to be the variable of state the wall, regarding a wall with n layers and

replacing the derivatives (differentials) by finite difference approximations, e. g. for layer 1, yields

$$\frac{dT_1}{dt} = \frac{\alpha}{\Delta x^2} (T_2 - 2T_1 + T_0) + \dot{q}_1 \quad (6)$$

and provides a reduction of the partial differential equations to a set of ordinary differential equations for the n layers, which may be written identically to equation (3).

The disturbance variables of the walls are the temperatures of the neighbour room and, for example the solar radiation to the walls. They are notified in the equations for the outer layer of the walls.

Since mathematical description of the state equations of all components of the system may be handled identically, the matrix equations of each physical component can be combined in one matrix equation of the total system, which is

$$\begin{aligned} & \dot{\mathbf{x}} = \mathbf{A}\mathbf{x} + \mathbf{B}\mathbf{u} \\ & \mathbf{y} = \mathbf{C}\mathbf{x} + \mathbf{D}\mathbf{u} \end{aligned}$$

where \mathbf{x} is the state vector, \mathbf{u} is the input vector, \mathbf{y} is the output vector, \mathbf{A} , \mathbf{B} , \mathbf{C} , and \mathbf{D} are matrices of appropriate dimensions. The matrices \mathbf{A} and \mathbf{B} are determined by the physical parameters of the system, while \mathbf{C} and \mathbf{D} are determined by the output equations. The matrices \mathbf{A} and \mathbf{B} are square matrices of order n , where n is the number of state variables. The matrices \mathbf{C} and \mathbf{D} are rectangular matrices of order m , where m is the number of output variables. The matrices \mathbf{A} and \mathbf{B} are determined by the physical parameters of the system, while \mathbf{C} and \mathbf{D} are determined by the output equations. The matrices \mathbf{A} and \mathbf{B} are square matrices of order n , where n is the number of state variables. The matrices \mathbf{C} and \mathbf{D} are rectangular matrices of order m , where m is the number of output variables.

$$= (a_{I,I} \ a_{I,AW} \ a_{I,IW} \ a_{I,H}) \cdot \begin{bmatrix} \vartheta_I \\ \vartheta_{AWo} \\ \vartheta_{IWo} \\ \vartheta_H \end{bmatrix} + (b_{I,A} \ b_{I,int}) \cdot \begin{bmatrix} \vartheta_A \\ \dot{Q}_{int} \end{bmatrix} \quad (2)$$

This equation can be translated into a vector equation (matrix representation)

$$\frac{d\Theta_I}{dt} = A_{I,j} \cdot \Theta_j + B_{I,j} \cdot s_j \quad (3)$$

with

- $A_{I,j}$ matrix of state
- Θ_j vector of state variables
- $B_{I,j}$ matrix of disturbance
- s_j vector of disturbance variables

The coefficients $a_{I,j}$ and $b_{I,j}$ of the influence coefficients of matrix $A_{I,j}$ and $B_{I,j}$ result from the heat transfer coefficients and heat capacities, for example

$$a_{I,AW} = \frac{a_k \cdot A_{AW}}{m_I \cdot c_I} \quad (4)$$

The partial differential equation of the transient heat transfer in the walls (Fourier's law) is

$$\frac{d\vartheta}{dt} = a \cdot \frac{\delta^2 \vartheta}{\delta x^2} \quad (5)$$

Discrete representation of the local differential coefficient of the temperature, assumed to be the variable of state of the wall, regarding a wall with n layers and replacing the derivatives (differentials) by finite difference approximations, e.g. for layer i , yields

$$\frac{d\vartheta_i}{dt} = \frac{a}{\left(\frac{\delta}{n}\right)^2} \cdot (\vartheta_{i-1} - 2\vartheta_i + \vartheta_{i+1}) \quad (6)$$

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set of coupled ordinary differential equations for the state variables of the total system, the state matrix equation,

$$\frac{dO_i}{dt} = \sum_{j=1}^n a_{ij} O_j + A_j + s_j \quad (7)$$

with

$$i, j = 1, 2, \dots, n$$

The time derivation of the state variables is a function of the state variables O_j and the disturbance variables s_j .

The state vector O contains the temperatures of the system components and the interference vector s contains the climatological data, respectively the temperatures of the neighbouring rooms, which are not simulated.

Any other component k of the total system-1 may be considered by determining the coefficients a_{kj} and b_{kj} (see equ. 2 and 3) and combining them to the matrix equation of the total system (see equ. 7).

The governing system of coupled ordinary differential equations, can be solved directly, without iteration, using highly stable implicit integration schemes with automatic time step control, generated by the margin of error estimate, for example semi-implicit Runge-Kutta methods, Gear's method, or orthogonal collocation method, yielding accurate and fast results.

3. HVAC System Simulation

3.1 Building Simulation

Base for simulation was a 4-room-residence model, fig. 3, consisting of 4 rooms, each with 2 outer walls, 2 inner walls and 2 windows. The residence is embedded in the middle of a multistorey building, where is assumed to have no heat transmission to neighbouring residences. Ceiling and floor are combined to one mass and are described by one differential equation in discrete representation.

The components are: Inner masses, heating, windows, walls.

Inner masses are the air and furniture as one mass with homogeneous temperature, which can absorb up to 15 W of the solar radiation; heat transfer occurs by convection, taking into account variable heat transfer coefficients.

Heating conditions are equal for each room. The radiator performance corresponds to standard heat requirement calculation. Control is according to indoor temperature as result of convection and radiation. Time constants of the rooms are between 70 h and 140 h.

"Solar windows" are regarded massless and therefore not represented in a differential equation; they operate as aperture for direct and diffusive solar radiation. Area of windows is varied from 0 - 40 % of total outer area of residence.

Walls are made from same material with same thickness. Solar radiation coming in is assumed to fall possibly on the walls. Outer and inner walls are discretely represented in 3 or 5 layers.

The first part of the document discusses the importance of maintaining accurate records of all transactions. It emphasizes that every entry should be supported by a valid receipt or invoice. This ensures transparency and allows for easy verification of the data.

In the second section, the author details the various methods used to collect and analyze the data. This includes both primary and secondary research techniques. The primary research involved direct observation and interviews with key stakeholders, while secondary research was conducted through a review of existing literature and industry reports.

The third section presents the findings of the study. It highlights several key trends and insights that emerged from the data analysis. These findings are presented in a clear and concise manner, using tables and charts where appropriate to illustrate the data points.

Finally, the document concludes with a series of recommendations based on the research findings. These recommendations are designed to provide practical guidance for the organization, helping it to address the challenges identified during the study and to capitalize on the opportunities that have been identified.

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Ceiling and floor are not discretely represented; heat is transferred only by conduction to neighbour residences. Heat is transferred at the surface by radiation and convection.

Internal heat sources are combined with the inner masses.

Heat transfer between components occurs by convection, radiation and conduction. Calculation of infrared-radiation regards all reflexions at the internal surfaces respecting the actual coefficients of emission conforming to the net-radiation method. Temperature control at day or night may be changed. The integration cycles are 10 min. or 1 h, after each of which heat transfer coefficients are recalculated. Air flow between rooms and outside may be controlled.

The program package balances energy for the reference model during the whole simulation time of a heating period, fig. 4.

The WSWO-model of the residence corresponds to building requirements according to WVO-law [31].

Improvement of insulation of outer walls from $k = 0,91 \text{ W/m}^2\text{K}$ to $k = 0,41 \text{ W/m}^2\text{K}$ has been realized.

Error balances were calculated for error tolerances 0.001, 0.01 and 0.1. Setting of program for simulation was: 0.1 / 5 layers / 10 m. Several physical and numerical tests passed with good results. Results have been gained for simulation periods of 1 h, 1 day, 1 week, 1 month and the whole heating period; energy amounts are shown in fig. 4. Different measures for energy saving had been taken into account: orientation and area, of windows, variable volume of rooms, standard insulation, translucent insulation, temporarily activated insulation of windows (TWS), triple-glass-windows, temperature drop at night individually for each room, air exchange between the rooms (constant or controlled). Free choice of material and windows is possible by introducing specific material constants. Different fixed space-heaters and simultaneously active heat sources simulate different usage of each room. Total energy consumption in function of different measures for heat-flow reduction is shown in fig. 5.

Highest reductions can be realized by increasing standard-insulation and by translucent insulation.

Different size of rooms makes little difference.

Combination of different measures in function of share of window-area is given in fig. 5.

Different methods of construction, e.g. weights, from lightweight to very heavyweight, influence energy consumption as shown in figs. 6 and 7.

Exploitation of solar radiation:

In case of solar radiation overheating of rooms by too much energy input might occur.

The extent of exploitation is given in fig. 8 in function of the share of window-area.

Comparing energy consumption for a model with translucent insulation results in nearly equalized energy balances between input and output.

Further results are published in [41], [5], [61].

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The program package balances energy for the reference model during the whole simulation time of a heating period, fig. 4.

The WSVO-model of the residence corresponds to building requirements according to WVO-law [3].

Improvement of insulation of outer walls from $k = 0,9 \text{ W/m}^2 \text{ K}$ to $k = 0,4 \text{ W/m}^2 \text{ K}$ has been realized.

Error balances were calculated for error tolerances 0.001, 0.01 and 0.1.

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Further results are published in [4], [5], [6].

3.2 Plant Simulation

3.2.1 Active and Passive Solar System

For a passive solar system, where heat capacity of the component glass can be neglected, the thermal balancing provides an algebraic equation

$$Q_{pass} = 190 \cdot A_F \cdot (T_{ff,r,f} - k_F - A_F - W_I - 9A) \quad (8)$$

which has to be merged into the main matrix of the total system and solved simultaneously. Validation by measurements for an active and a passive system is shown in fig. 9. Further results published in [7].

3.2.2 Thermal Storage System

3.2.2.1 Physical Model

The considered thermal storage (resign, fig. 10, is to be a thermally stratified upstream charge storage tank, equipped with constant heater performance.

Natural and forced convection of storage medium water are simulated by an additional equivalent coefficient

$$A, \text{qu}(t, Z) = h_{cond}(l @ Z) + h_{conv}(t @ Z) \quad (9)$$

Based on one-dimensional heat conduction and convection only the energy conservation balance can be regarded. Consequently the modelling results in the following scheme, fig. 10, with three level stratification: inlet, central, outlet level, which can be heated or not.

3.2.2.2 Mathematical formulation

Analogue to chapter 2.2 first of all the differential equation has to be established by setting up the energy balance of the mass within the storage tank.

The control volume represented in layers, yields the following equation

$$\rho \cdot c \cdot \frac{\partial T}{\partial t} \cdot \Delta Z = \rho \cdot c \cdot A \cdot (v \cdot T) - \rho \cdot c \cdot A \cdot (v \cdot T) + q' \cdot A \cdot \Delta Z \quad (10)$$

which gives with $AZ \rightarrow 0$ the differential equation of the storage system.

$$\rho \cdot c \cdot \frac{\partial T}{\partial t} = \rho \cdot c \cdot v \cdot \frac{\partial T}{\partial Z} - \rho \cdot c \cdot v \cdot \frac{\partial T}{\partial Z} + q' \quad (11)$$

Introducing Fourier's law of heat flow

(11)

... ..
... ..
... ..

$$\frac{1}{2} \frac{d}{dt} \left(\frac{1}{2} \frac{d^2}{dt^2} \right) = \frac{1}{2} \frac{d^3}{dt^3}$$

... ..

3.2 Plant Simulation

3.2.1 Active and Passive Solar System

For a passive solar system, where heat capacity of the component glass can be neglected, the thermal balancing provides an algebraic equation

$$\dot{Q}_{pass} = I_{90} \cdot A_F \cdot (\tau\alpha)_{F,eff} - k_F \cdot A_F \cdot (\vartheta_I - \vartheta_A) \quad (8)$$

which has to be merged into the main matrix of the total system and solved simultaneously.

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The considered thermal storage design, fig. 10, is to be a thermally stratified upstream charge storage tank, equipped with constant heater performance. Natural and forced convection of storage medium water are simulated by an additional equivalent heat-conduction coefficient

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Based on one-dimensional heat conduction and convection only the energy conservation balance has to be regarded. Consequently the modelling results in the following scheme, fig. 10, with three levels of stratification: inlet, central, outlet level, which can be heated or not.

3.2.2.2 Mathematical formulation

Analogue to chapter 2.2 first of all the differential equation has to be established by setting up the energy balance of the mass within the storage tank.

The control volume represented in layers, yields the following equation

$$\rho \cdot c \cdot \frac{\delta T}{\delta t} = - \frac{\dot{q}_{z+\Delta z} - \dot{q}_z}{\Delta z} - \frac{\dot{m} \cdot c}{A} \cdot \frac{T_{z+\Delta z} - T_z}{\Delta z} + \dot{q}_i \quad (10)$$

which gives with $\Delta z \rightarrow 0$ the differential equation of the storage system.

$$\rho \cdot c \cdot \frac{\delta T}{\delta t} = - \frac{\delta}{\delta z}(\dot{q}) - \frac{\dot{m} \cdot c}{A} \cdot \frac{\delta}{\delta z}(T) + \dot{q}_i \quad (11)$$

Introducing Fourier's law of heat flow

$$\dot{q} = -\lambda \cdot \frac{\delta T}{\delta z} \quad (12)$$

is leading to the basis equation for simulation

$$\frac{dT}{dt} = -\left(\frac{A}{Z} + \frac{A}{Z} + \dots\right) T + q' \quad (13)$$

The solution of this parabolic differential equation needs two physical random and one time dependent i conditions.

Random conditions: The charging energy flow at the first layer of the storage tank is equal to the energy rate at entrance of the tank and consists of a convective and diffusive flux, and temperature i_{in} . The temperature gradient at the outlet must be equal to zero.

Initial condition: Initial temperature (~distribution) of the storage tank must be given, e.g. as constant temperature over the volume of the tank.

3.2.2.2 Numerical Solution

Reduction of the given partial differential equation of higher order for each point of definition to an ordinary differential equation of first order is analogous to 2.9 achieved by replacing the local differentials by quotients of differences, for point. The quotients of differences are determined from the temperatures of the discrete points of local coordinate. State space representation gives a reduction of the basis equation; introduction of the above mentioned quotient differences leads to the desired and from 2.2 well known matrix representation. Thus the matrix of state for a the storage tank with variable number of layers is containing only the temperatures of the layers as state variables and temperatures of cold water inlet and heater performance as interference variables. Conforming to the development of a general program in 2.2 the restructuring

of the ordinary differential equation of first, order allows the very clear

matrix representation which may be solved as stand alone program or merged into the main matrix of state equation the total system together with the other components and the building.

$$\frac{dO_j}{dt} = A_{i,j} O_j + B_{i,j} s_j \quad (14)$$

3.2.2.3 Results

Numerical results have been validated by comparing them with analytically deduced solutions.

Verification by help of experiments is shown in figs. 11 and 12.

Future works will concentrate on enlarging the model libraries and on increasing the efficiency and ease of use to meet the demands of HVAC application.

is leading to the basis equation for simulation

$$\rho \cdot c \cdot \frac{\delta T}{\delta t} = -\frac{\delta}{\delta z} \left(-\lambda \cdot \frac{\delta T}{\delta z} \right) - \frac{\dot{m} \cdot c}{A} \cdot \frac{\delta}{\delta z} (T) + \dot{q}_i \quad (13)$$

The solution of this parabolic differential equation needs two physical random and one time dependent initial conditions.

Random conditions: The charging energy flow at the first layer of the storage tank is equal to the energy rate at the entrance of the tank and consists of a convective and diffusive share, and temperature $\vartheta_{\infty}^{in} = \vartheta_{in}$. The temperature gradient at the outlet must be equal to zero.

Initial condition: Initial temperature (-distribution) of the storage medium must be given, e.g. as constant temperature all over the volume of the tank.

3.2.2.2 Numerical Solution

Reduction of the given partial differential equation of higher order for each point of definition to an ordinary differential equation of first order is analogue to 2.2 achieved by replacing the local differentials by quotients of differences for each point. The quotients of differences are determined from the temperatures of the discrete points of local coordinate.

State space representation gives a reduction of the basis equation; introduction of the above mentioned quotients of differences leads to the desired and from 2.2 well known matrix representation. Thus the matrix of state for a thermal storage tank with variable number of layers is containing only the temperatures of the layers as state variables and the temperatures of cold water inlet and heater performance as interference variables.

Conforming to the development of a general program modul in 2.2 the restructuring of the ordinary differential equation of first order allows the very clear matrix representation which may be solved as stand alone program or merged into the main matrix of state equations of the total system together with the other components and the building.

$$\frac{d\Theta_i}{dt} = A_{i,j} \cdot \Theta_j + B_{i,j} \cdot s_j \quad (14)$$

3.2.2.3 Results

Numerical results have been validated by comparing them with analytically deduced solutions.

Verification by help of experiments is shown in figs. 11 and 12.

Future works will concentrate on enlarging the model libraries and on increasing the efficiency and ease of use to meet the demands of HVAC application.

4. Literature

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5. Nomenclature:

Indices:

A	outdoor, outside
akt	active
A 11'	otiter wall
B	floor
F	wallow
H	heating system, radiator
1,1 j	rminhig index of variables of stale and disturbance
l111	inner wall
L	air
771(13,	MaXI111111111
NR	neighbour room

•	surface
pass	passive
801	solar
1,11	flow (pipe)
R	rettirn (pipc)

4. Literature

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5. Nomenclature:

Indices:

<i>A</i>	outdoor, outside
<i>akt</i>	active
<i>AW</i>	outer wall
<i>B</i>	floor
<i>F</i>	window
<i>H</i>	heating system, radiator
<i>i, j</i>	running index of variables of state and disturbance
<i>IW</i>	inner wall
<i>L</i>	air
<i>max</i>	maximum
<i>NR</i>	neighbour room
<i>o</i>	surface
<i>pass</i>	passive
<i>sol</i>	solar
<i>V</i>	flow (pipe)
<i>R</i>	return (pipe)

Formulary

a	$7711'ls$	thermal diffusivity
ai,j	lls	coefficients of inatrix Ai,j
AF	$771 \ 2$	area, of window
Ai,j	-	matrix of state vector
bi,j	lls	coefficients of niatrix Bi,j
Bi,j		matrix of disturbance vector
c	$J1kgE$	heat capacity
cpL	$J1kgK$	lheat capacity of air at constant pressure
$,go$	R'/in'	solar radiation to a vertical surface
k	$iT'in'K$	heat transmission coefficient
777	kg	inass
$1P I$	kg	inner masses
71		number of discrete wall layers, number of systemi-components

A. TV heat flow

Q	$A. IV h$	energy
$Qakt$	$4.11'h$	energy of active solar system
$Qges$	$A.IVh$	total energy loss (energy supply
QII	$A.Wh$	Heating energy of Heating system
$Qint$	$k 1V h$	energy of internal sources
$0Norm$	OV	standard heat requirement
$QSol$	$017h$	solar radiation into rooin
lq	771	thickness of wall
t	8	time
	771	local coordinate
$.r$		
$(v$	$TV/in'K$	factor of absorption
Cyk	$IT'in'K$	convective licat transfer coefficient
$Q,$	$W1777'K$	heat transfer coefficient of radiation
T		coefficient of transmission
		coefficient of solar capacity of energy
71	-	efficiency
9	$0 (1,$	temperature
g	OC	indoor temperature
$1) A$	oc	outdoor temperature
01		parameter of control

Formulary

a	m^2/s	thermal diffusivity
$a_{i,j}$	$1/s$	coefficients of matrix $A_{i,j}$
A_F	m^2	area of window
$A_{i,j}$	—	matrix of state vector
$b_{i,j}$	$1/s$	coefficients of matrix $B_{i,j}$
$B_{i,j}$	—	matrix of disturbance vector
c	J/kgK	heat capacity
c_{pL}	J/kgK	heat capacity of air at constant pressure
I_{90}	W/m^2	solar radiation to a vertical surface
k	W/m^2K	heat transmission coefficient
m	kg	mass
m_I	kg	inner masses
n	—	number of discrete wall layers, number of system-components
\dot{Q}	kW	heat flow
Q	kWh	energy
Q_{akt}	kWh	energy of active solar system
Q_{ges}	kWh	total energy loss (energy supply)
Q_H	kWh	heating energy of heating system
Q_{int}	kWh	energy of internal sources
Q_{Norm}	kW	standard heat requirement
Q_{sol}	kWh	solar radiation into room
s	m	thickness of wall
t	s	time
x	m	local coordinate
α	W/m^2K	factor of absorption
α_k	W/m^2K	convective heat transfer coefficient
α_s	W/m^2K	heat transfer coefficient of radiation
τ	—	coefficient of transmission
ϵ	—	coefficient of solar capacity of energy
η	—	efficiency
ϑ	oC	temperature
ϑ_I	oC	indoor temperature
ϑ_A	oC	outdoor temperature
σ	—	parameter of control

HVAC-system

time.

-J Int. licat sources

air Heading system

1F-

solar system

a
l

CD
mass

storage -SY-S-te-M

U
Or

>

(D

QP4S

F'

J passive system

floor
building

d wait delay.
floor

Fig. 1 Control system chart

AW, A

GIWAW

wal
l

dI,AW

internal mass

L

outdoor

GM, F

-01M

window
indoor

F, A

So[

'de wall

C-

0 H,1

outsi

radiator

lant -----

'Jeso It

radiation

c
o
n
v
e
c
t
i

FIR. 2 Enemy finw chart



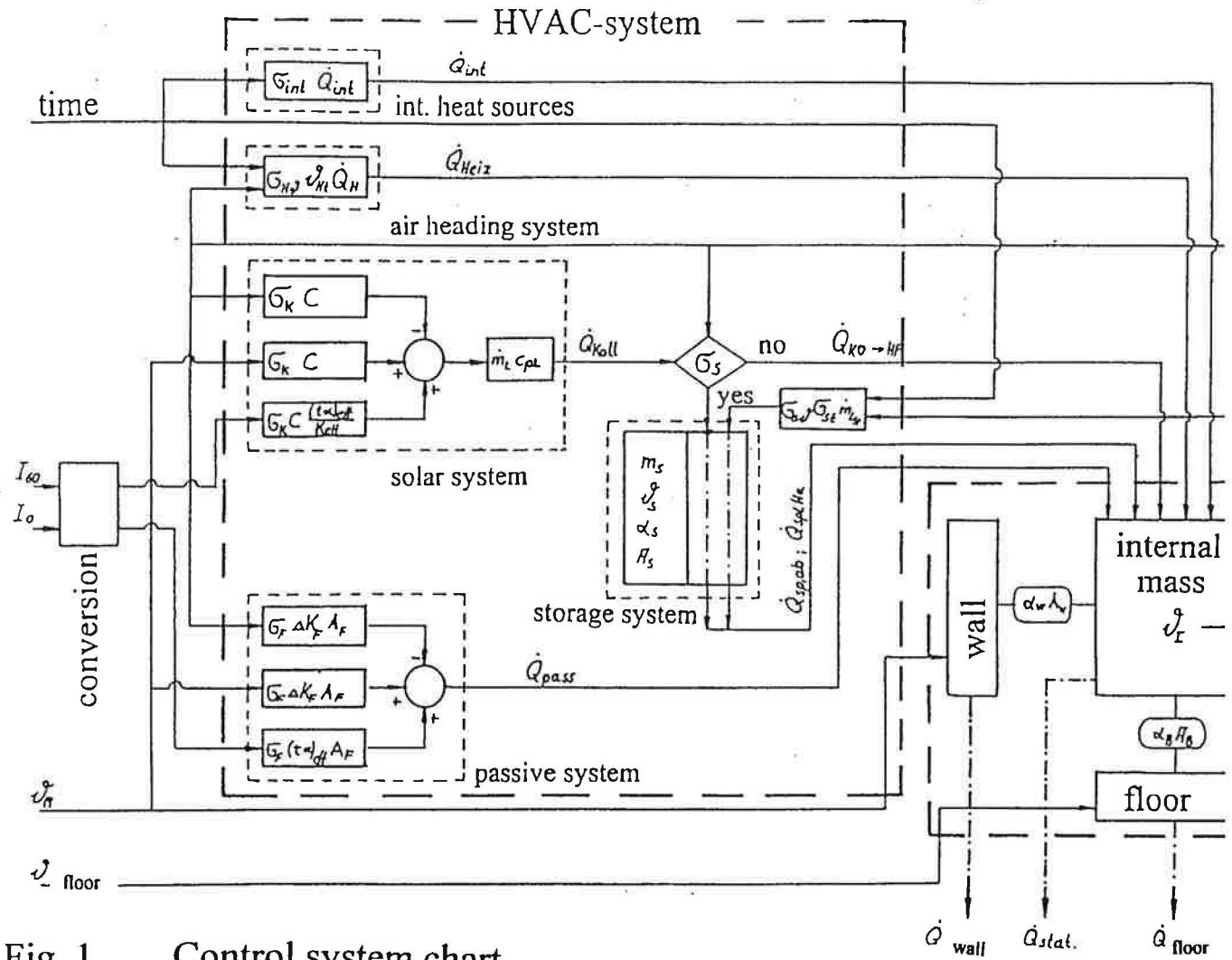
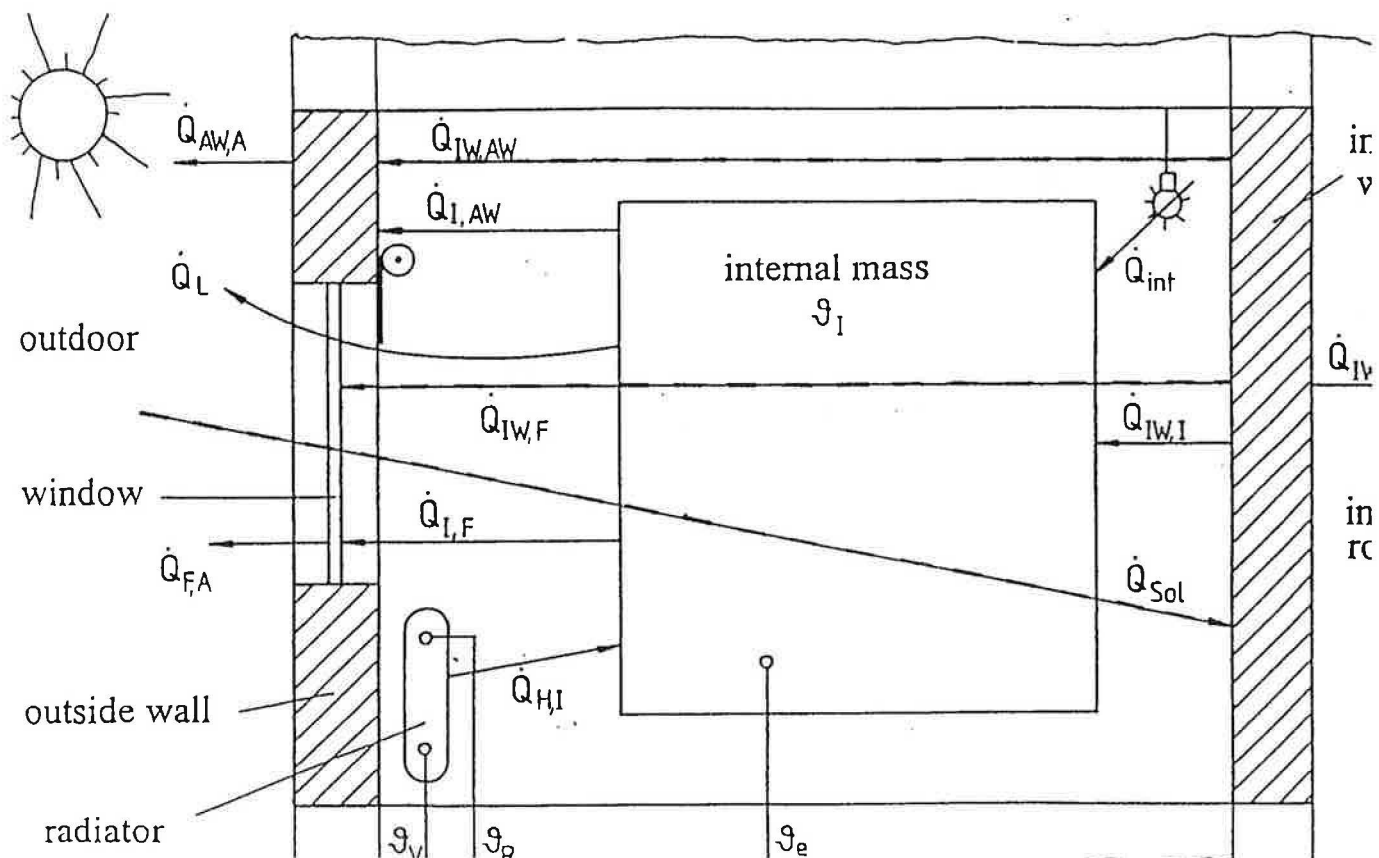


Fig. 1 Control system chart



W eiz

QUeb

QLmin

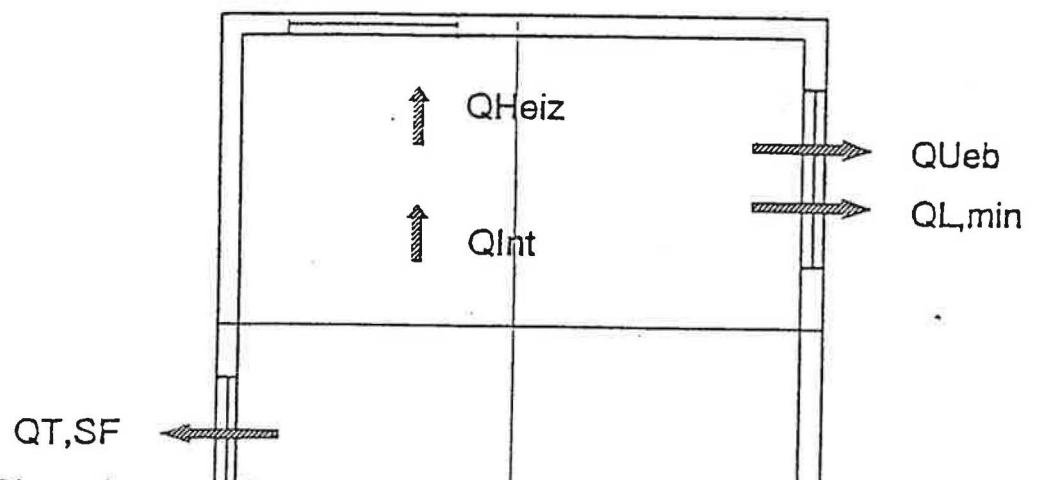
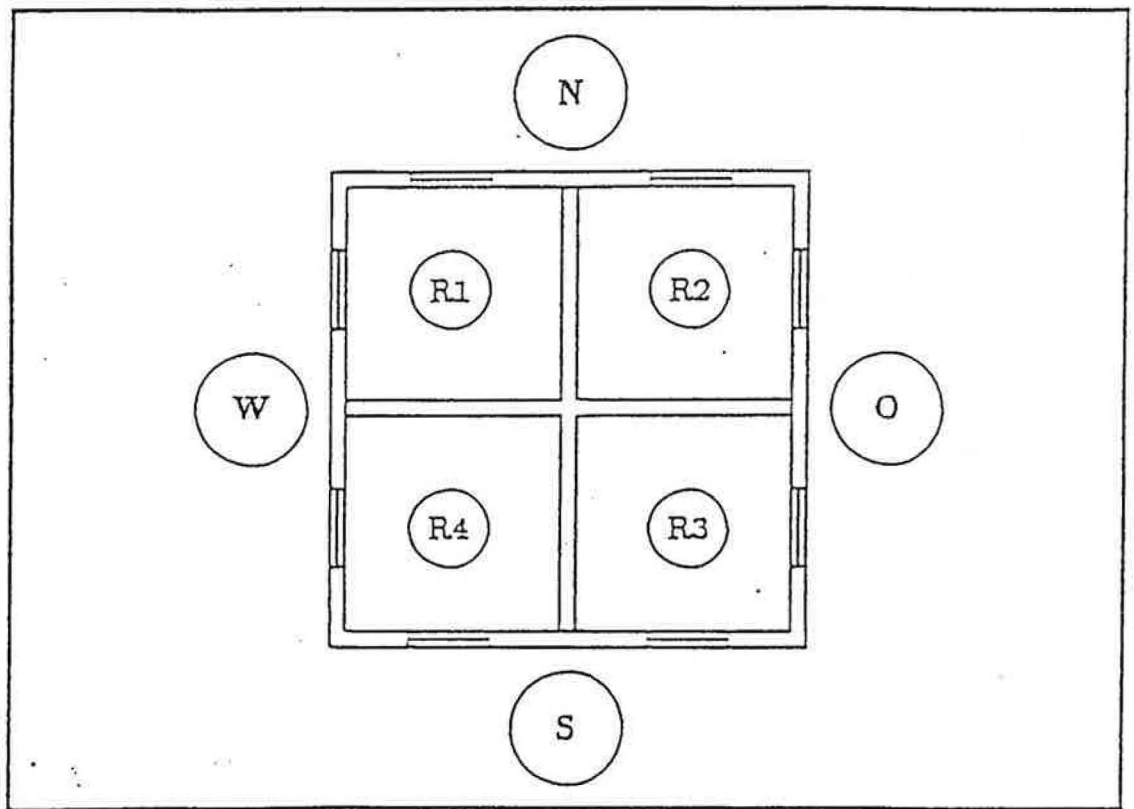
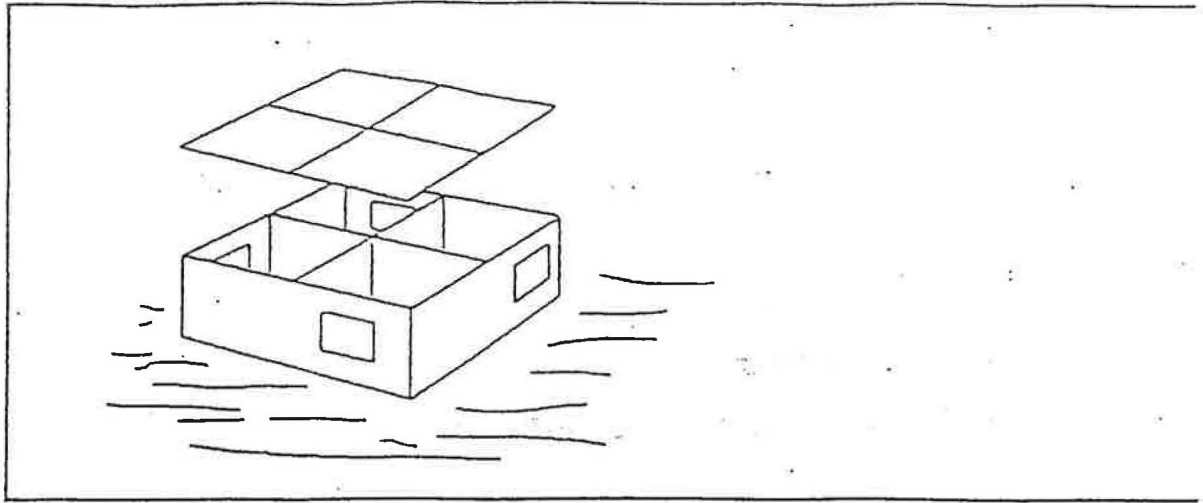
QT, S F

CLnuz,f

QT,W,A

Fig. 3 Building: 4-room-model





Reference model: energy saving

WWO

insulation S TWS
triple-glas'

Q f kWhl

12000 -

10000

8000 4-

6000

4000

2000

0

Heiz Ant Inuzi TSF *Lmin* Ueb

Reference model: heating energy

QK [kWhl

14000

13000

U"

12000 -

C)

11000

10000

9000

8000

C2
ZE

CI)

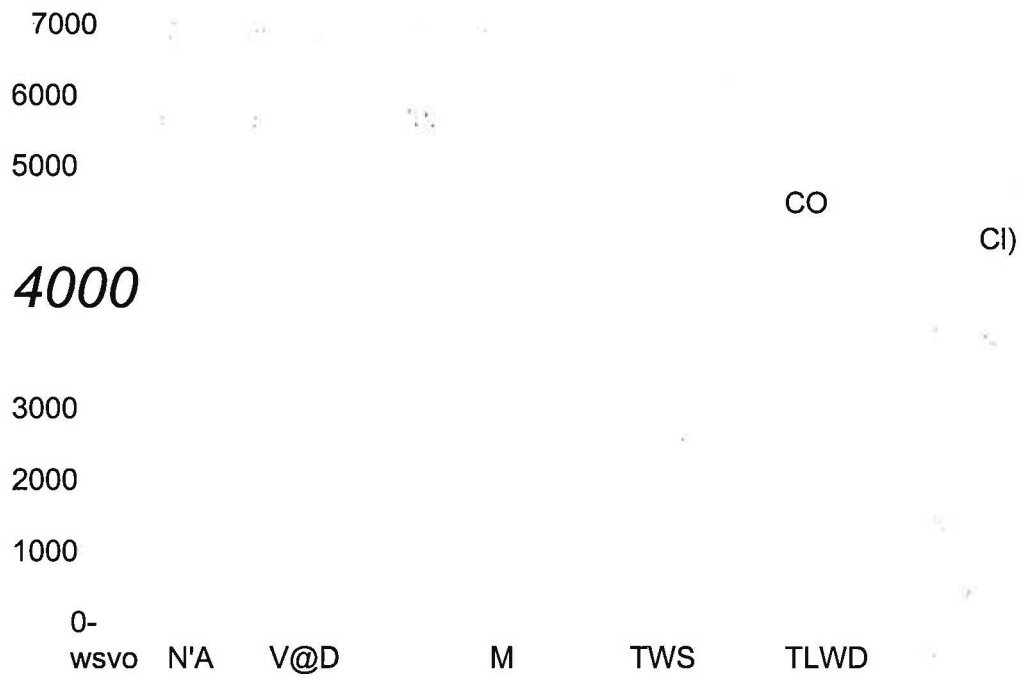
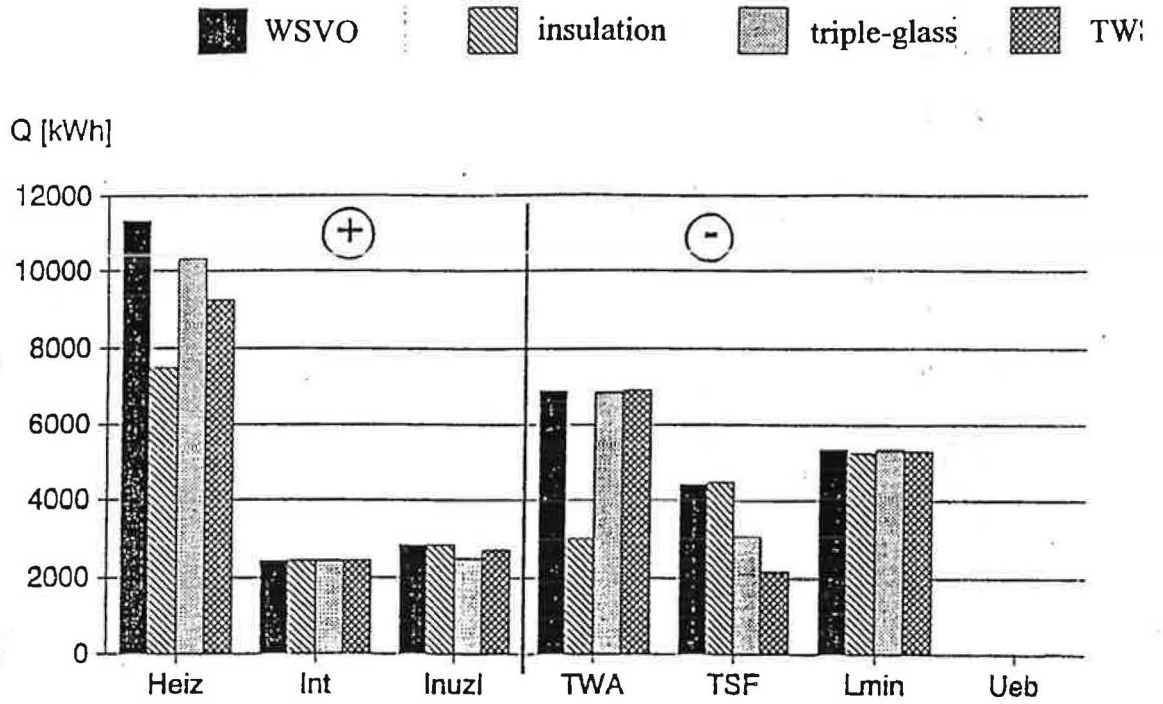
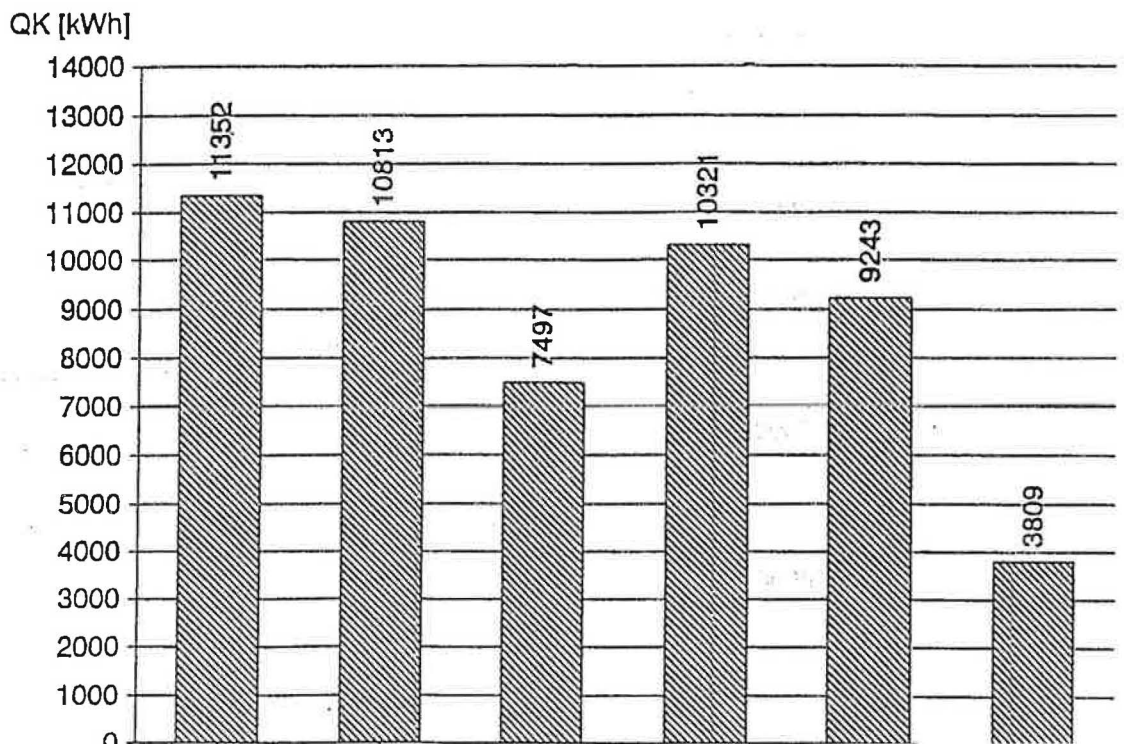


Fig. 4

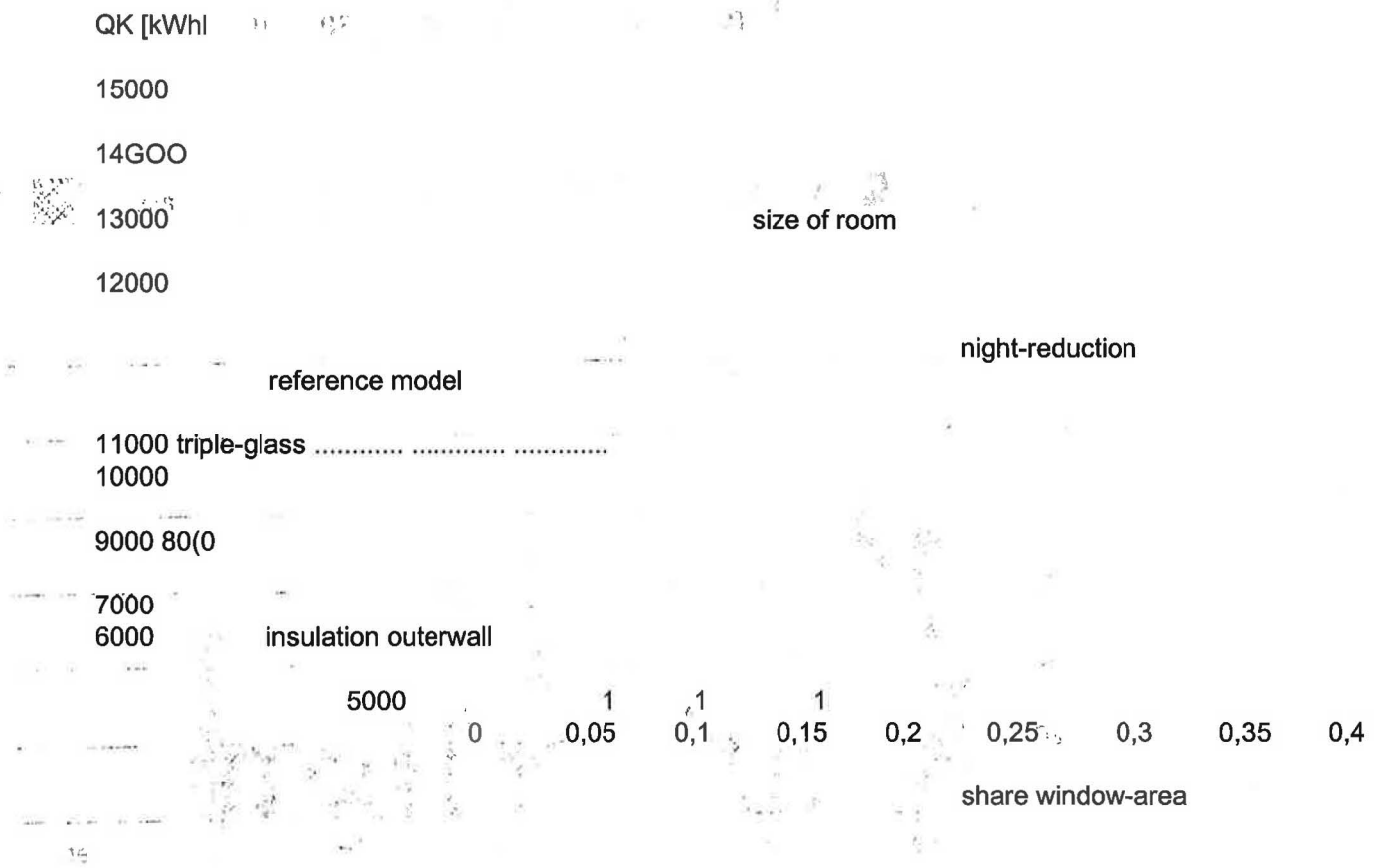
Reference model: energy saving



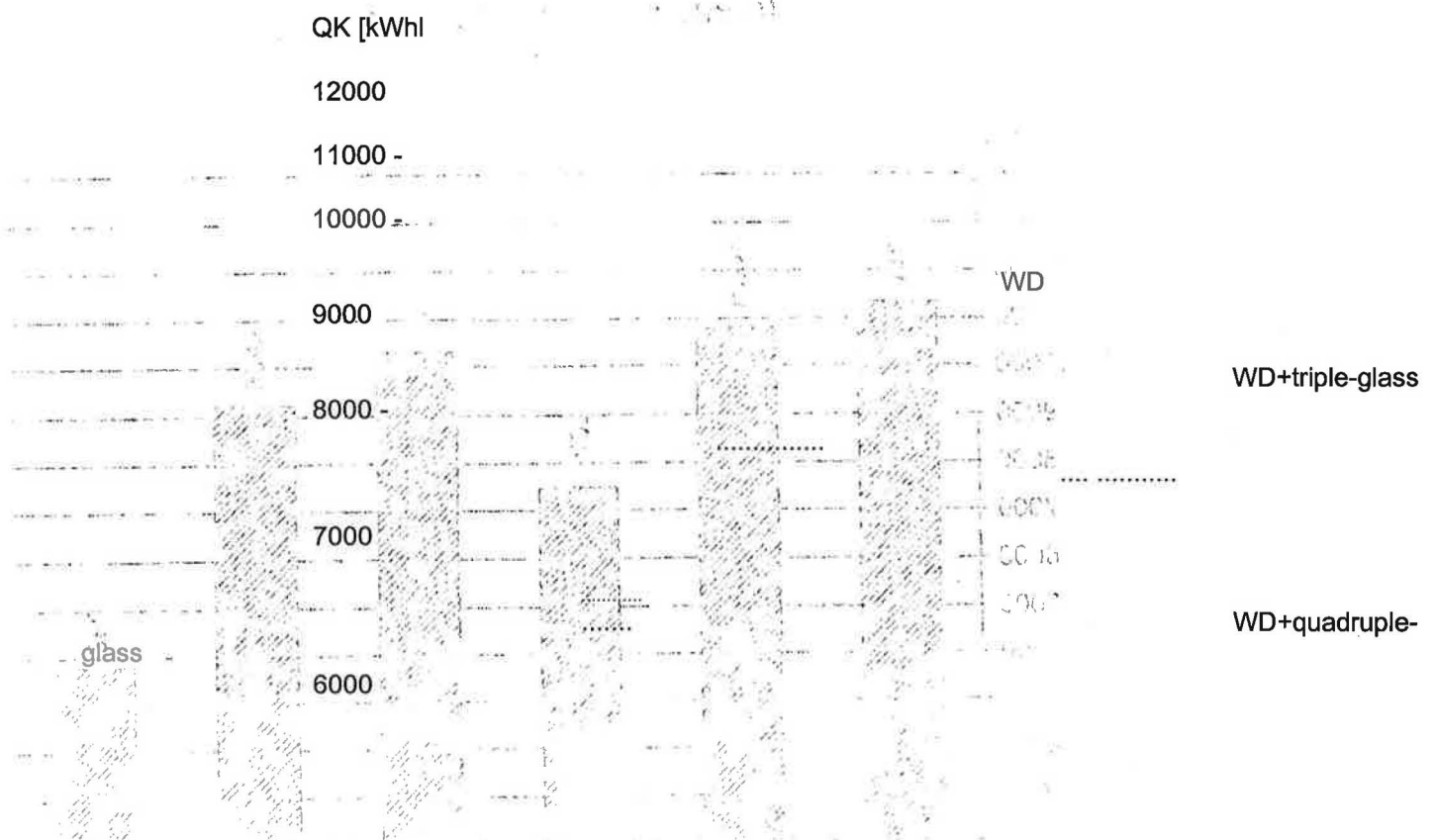
Reference model: heating energy



Energy saving, separate



Energy saving, combined



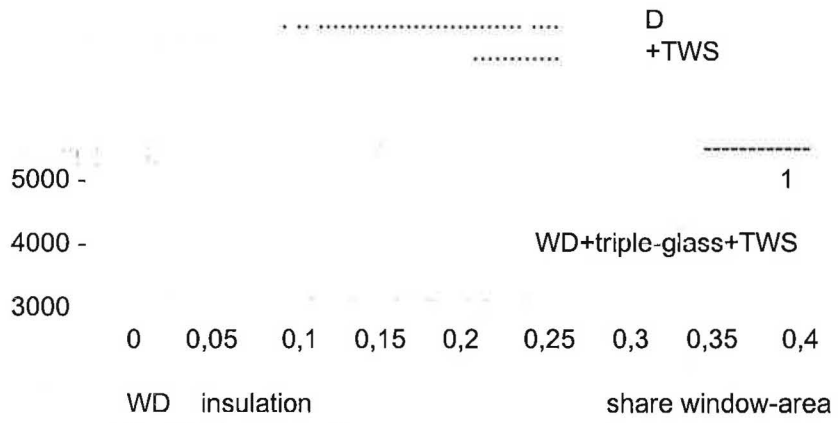
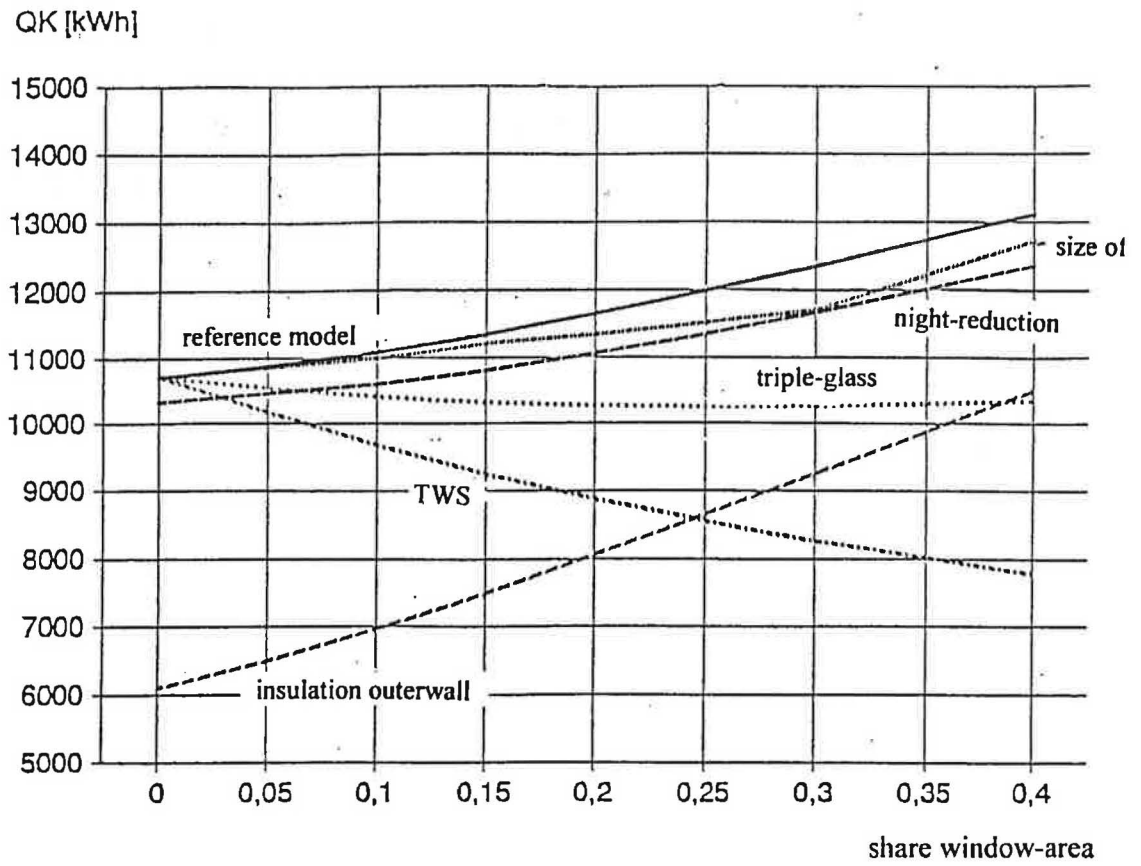
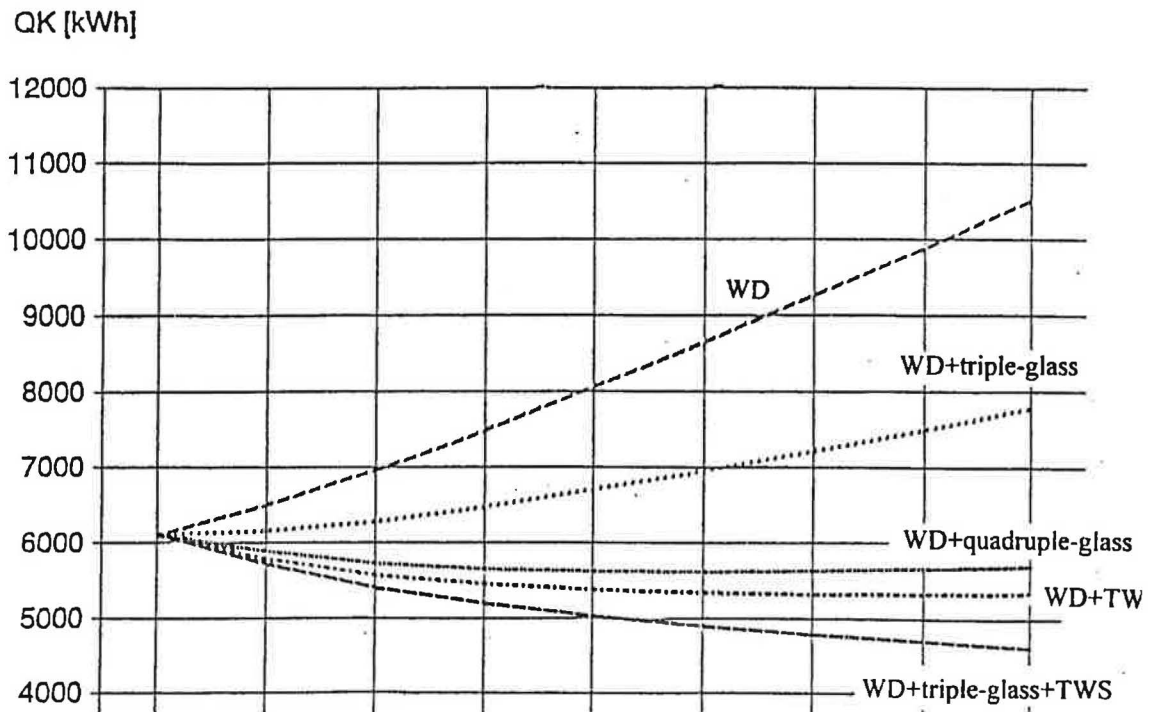


Fig. 5

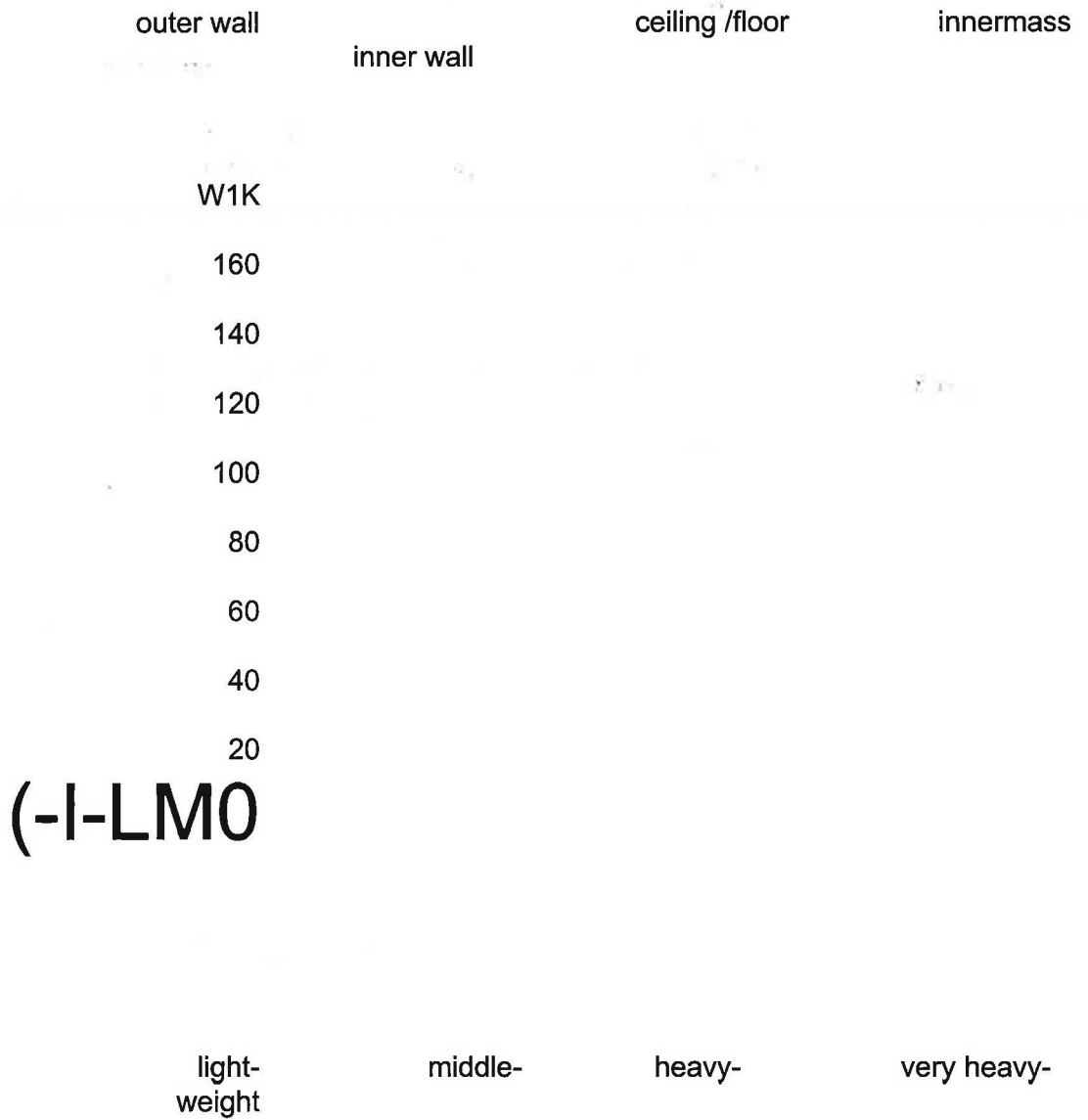
Energy saving, separate



Energy saving, combined



Construction: heat capacity
 MRK)share of window area 0, 15



Construction: comparison

weight

110(0
 10500 -

light wei
 middle

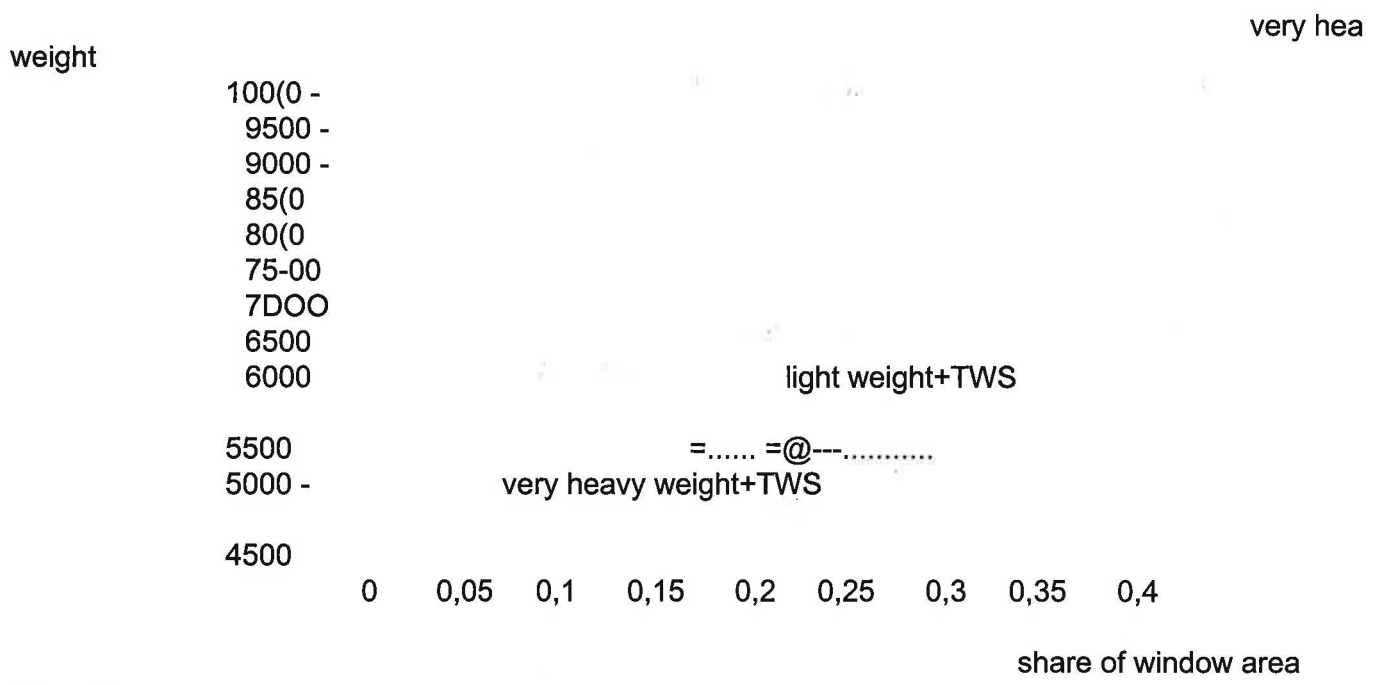
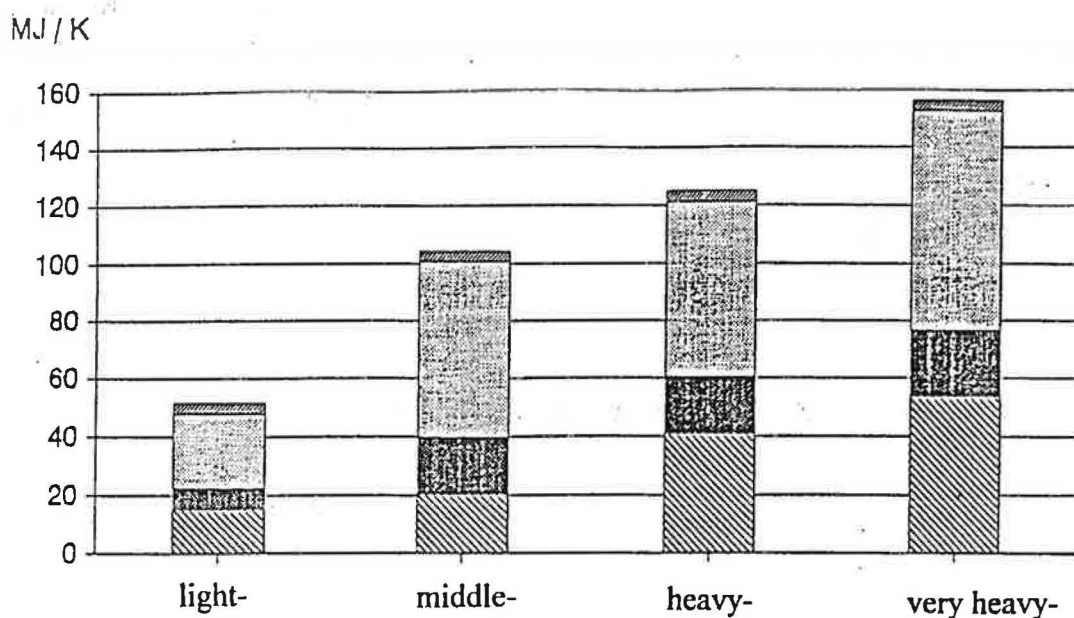


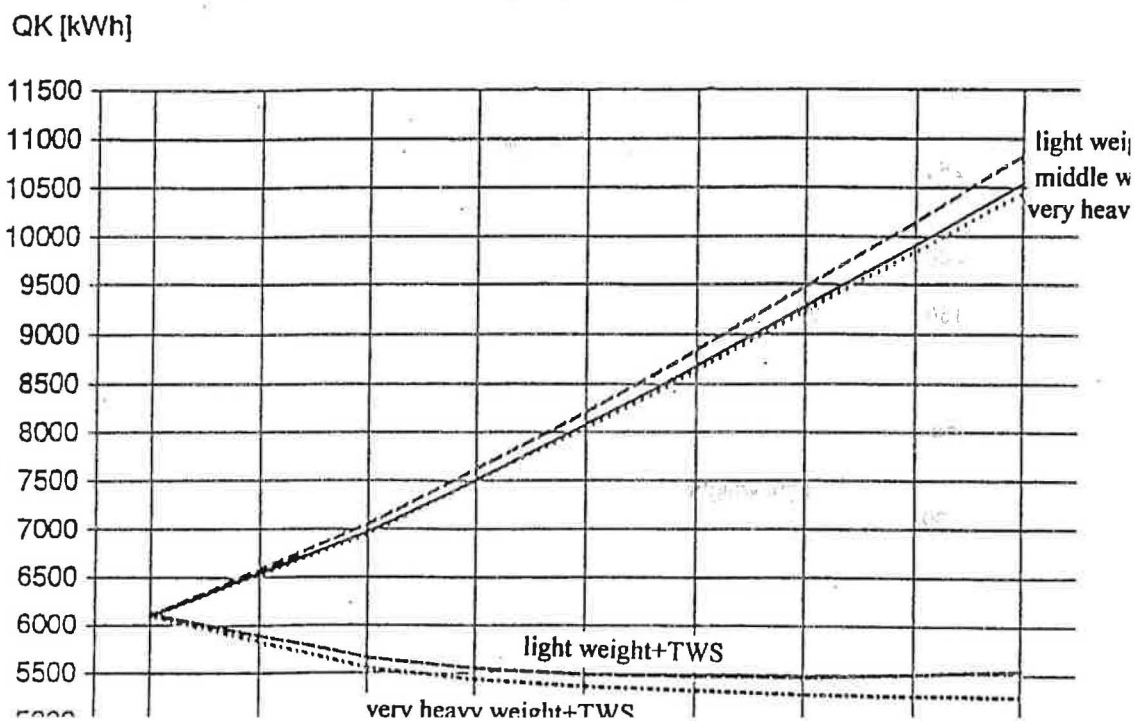
Fig. 6

Construction: heat capacity (MJ/K) share of window area 0,15

outer wall
 inner wall
 ceiling /floor
 innermass



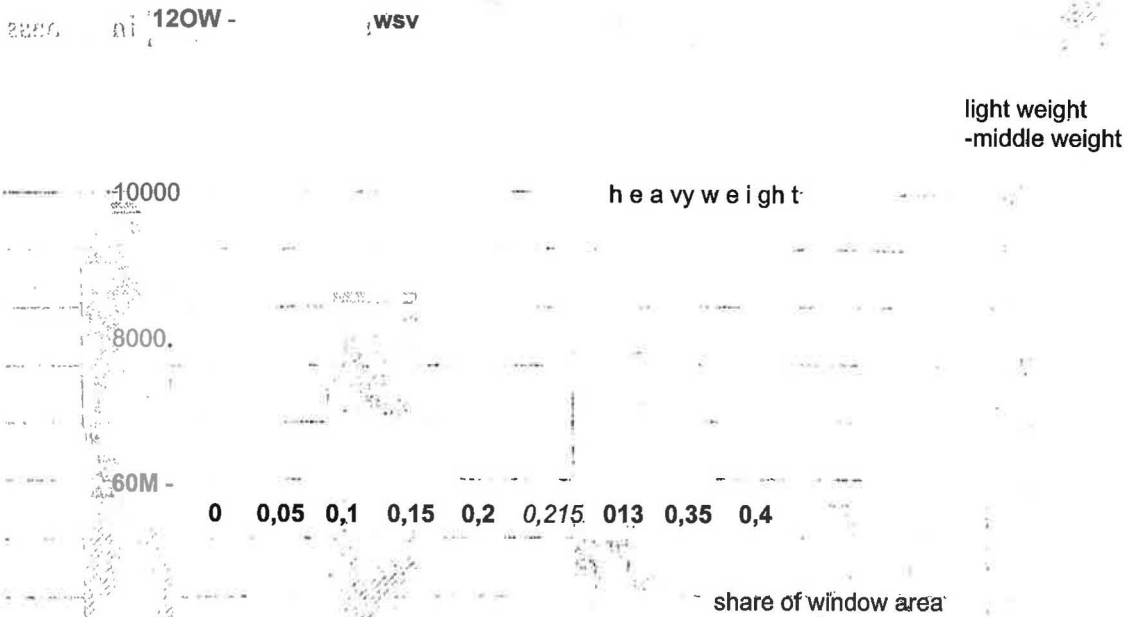
Construction: comparison



Construction: heating energy

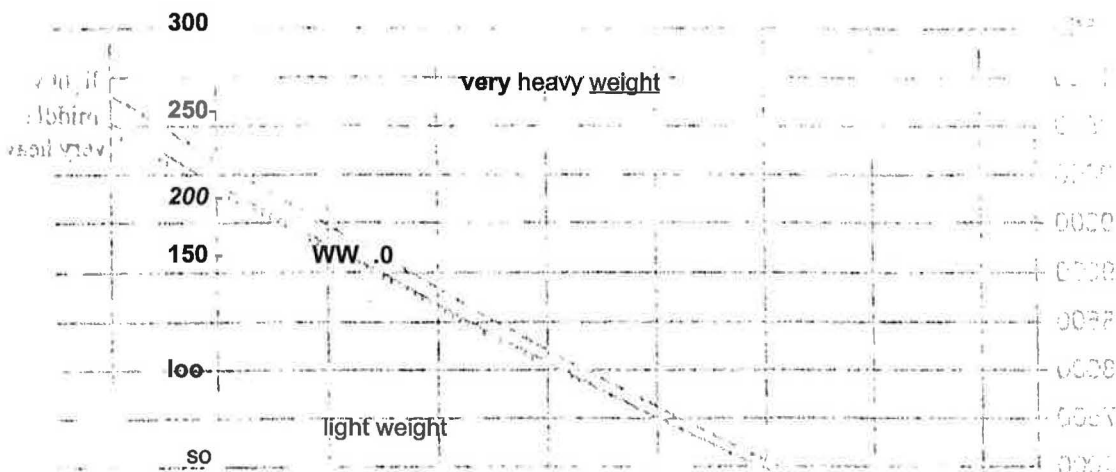
Q [kWh] Reference model (WSVO
insulation of outer wall construction with

14000.



Construction: time constant

T [h]



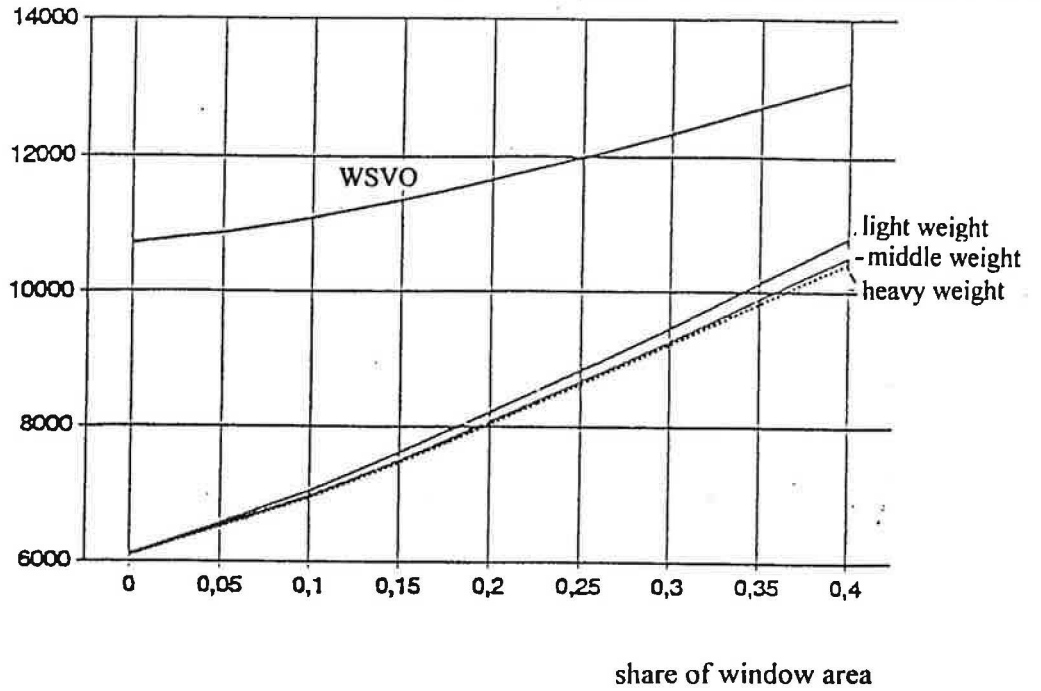
0
 0 0,05 0,1 0,15 0,2 0,25 **0,3** 0,35 0,4
 share of window area

Fig. 7



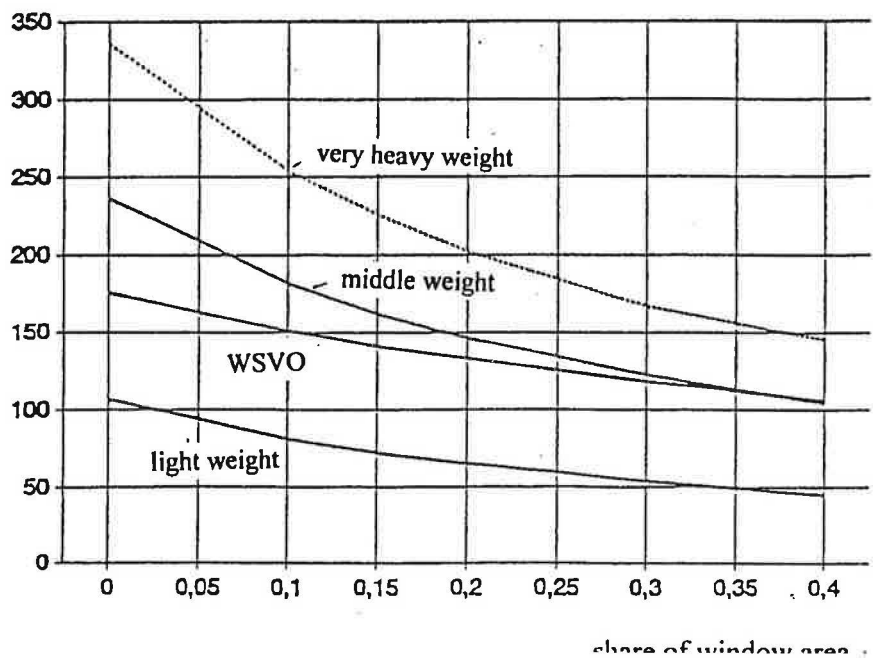
Construction: heating energy

Q [kWh] Reference model (WSVO); construction with insulation



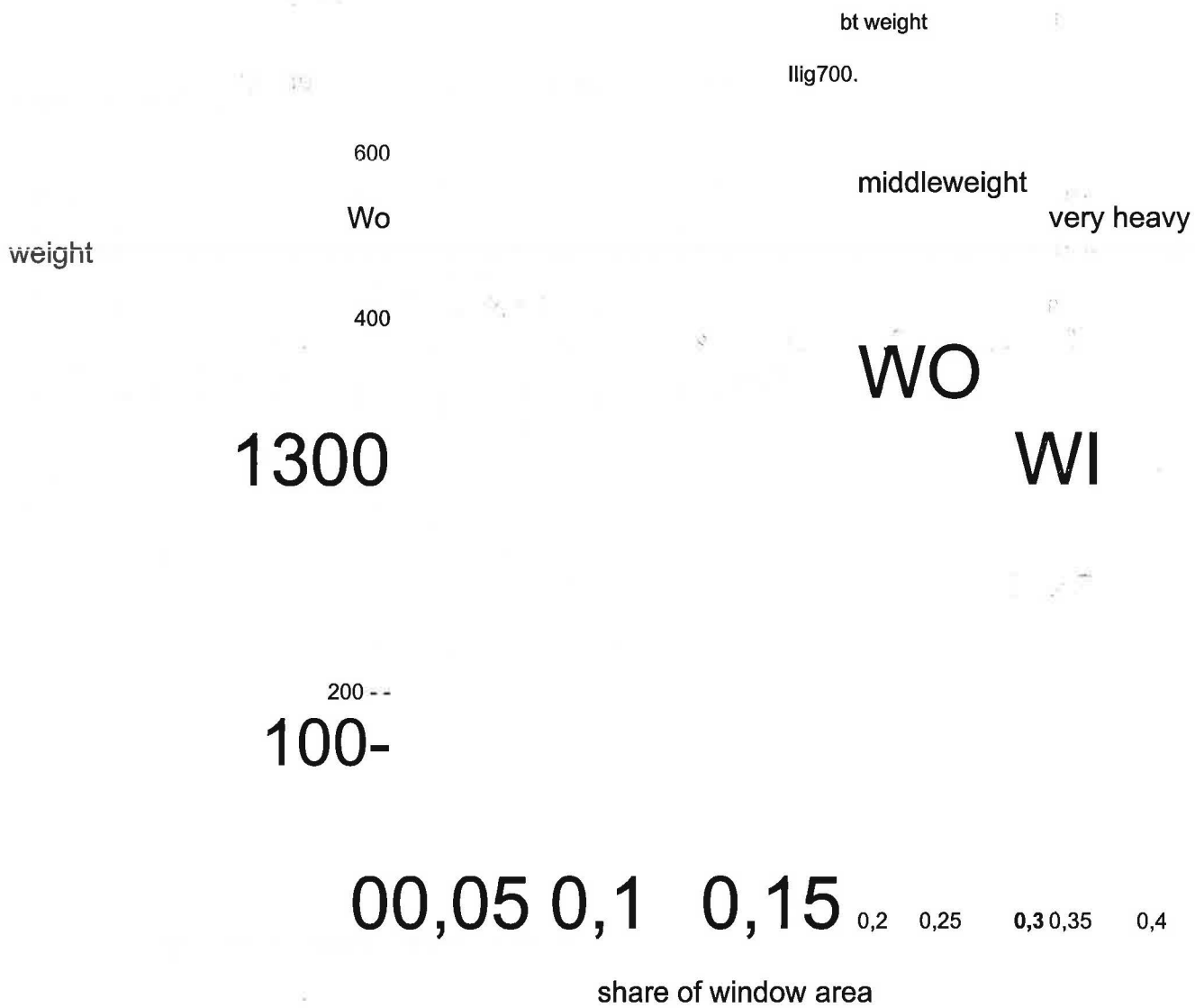
Construction: time constant

T [h]



Solar energy: surplus

Q[kWh] Ref model (WSVO); construction with insulation of outer wall



Solar energy: exploitation effectiveness

0,96

0,95

0,94

0,93

0,92

0,91

0,9

0 0,05 0,1 0,15 0,2 0,25 0,3 0,35 0,4

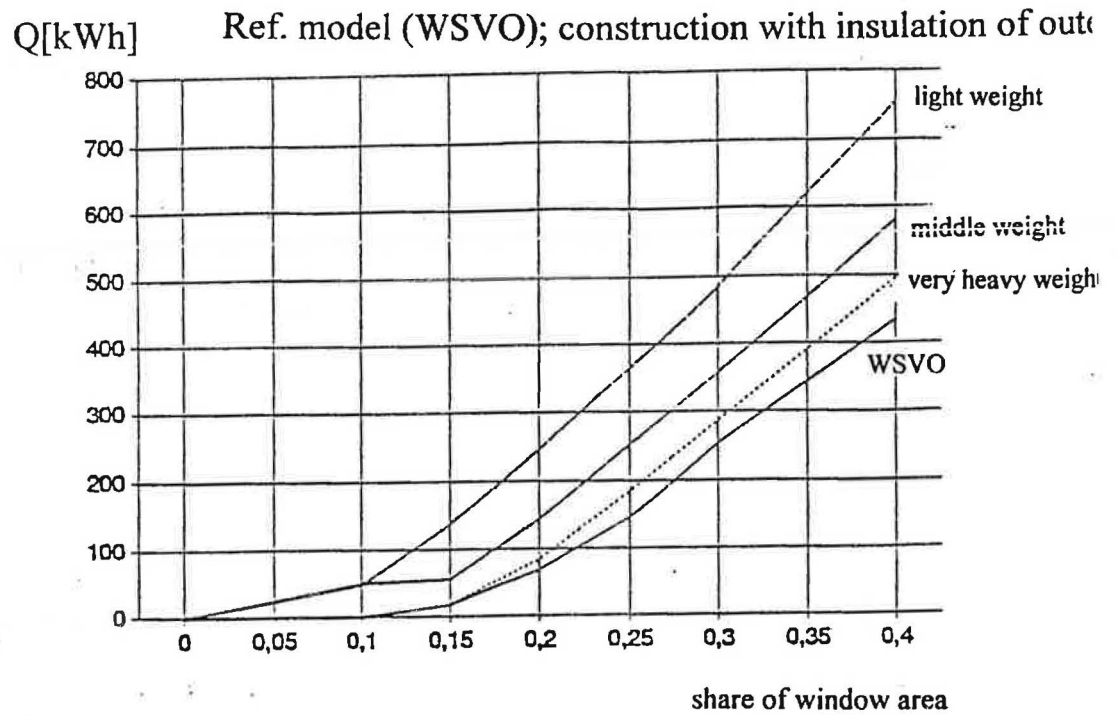
t weight

WVO

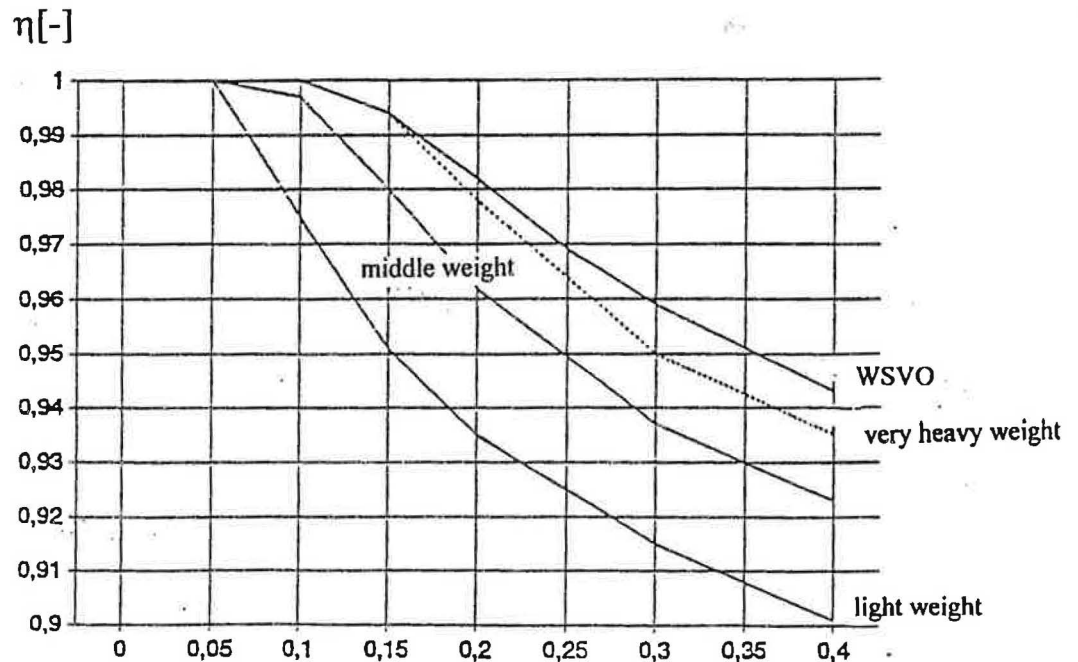
very heavy weight

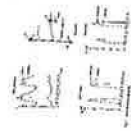
Fig. R

Solar energy: surplus

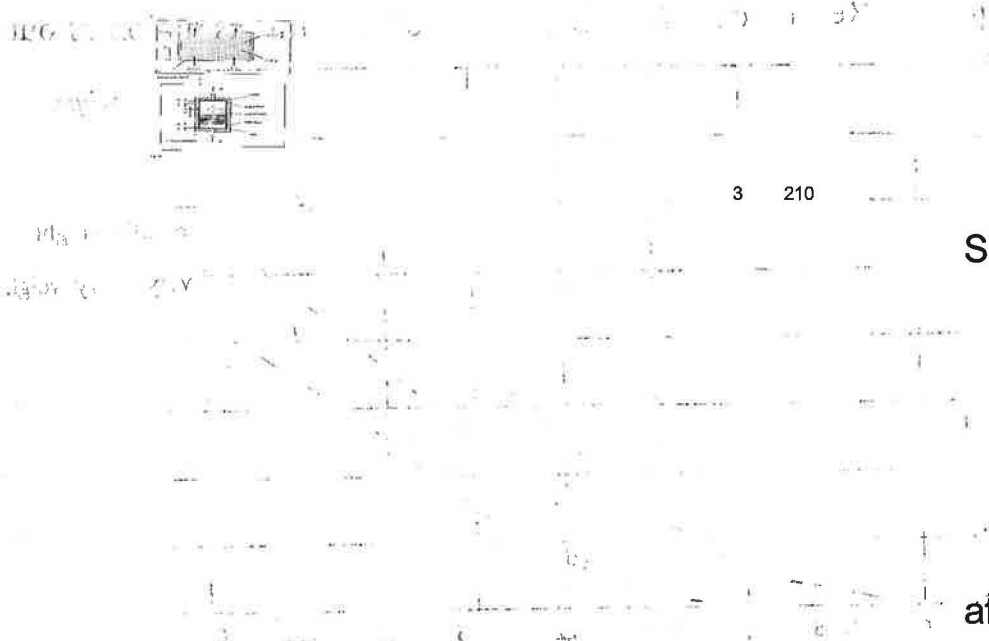


Solar energy: exploitation effectiveness





170 835



3 210

Storage tank

after 10 minutes charging

N 1800 -

1200 -

1500

900 -

600 -

300 -

